R13.2 Internal-Age Distribution, $I(\alpha)$

The relationship between the *internal-age* and *external-age distribution* can be demonstrated by analyzing a continuous reactor operating at steady state that is filled with material of volume V. Consider again that the volume of reactor is filled with maize-colored molecules, and at time t = 0 we start to inject blue molecules to replace the maize molecules. By definition of $I(\alpha)$, the volume of molecules inside the reactor that have been there between a time α and $\alpha + d\alpha$ is

$$dV = V[I(\alpha)] d\alpha \tag{R13.2-1}$$

At t=0 we will let $(v_0 d\alpha)$ be the first volume of blue molecules that enter the reactor. We want to consider what has happened to the molecules in this volume at a time α after being injected. Some of the molecules will already have left the system at a time α , while others remain. The fraction of molecules that still remain in the system is $[1-F(\alpha)]$. Consequently, the volume of molecules that entered the system between t=0 and $t=d\alpha$ and are still in the system at a later time α is

 $dV = v_0 d\alpha [1 - F(\alpha)] \tag{R13.2-2}$

This is the volume of molecules that have an age between α and $(\alpha + d\alpha)$. Equating Equations (R13.2-1) and (R13.2-2) and dividing by V and by $d\alpha$ gives

$$I(\alpha) = \frac{v}{V} \left[1 - F(\alpha) \right]$$

Then

Relating $I(\alpha)$ to $F(\alpha)$ and $E(\alpha)$

$$I(\alpha) = \frac{1}{\tau} \left[1 - F(\alpha) \right] = \frac{1}{\tau} \left[1 - \int_0^\alpha E(\alpha) \, d\alpha \right]$$
 (R13.2-3)

Differentiating Equation (R13.2-3) and noting that

$$\frac{d[1-F(\alpha)]}{d\alpha} = -E(\alpha)$$

gives

$$E(\alpha) = -\frac{d}{d\alpha} \left[\tau I(\alpha) \right]$$
 (R13.2-4)

As a brief exercise, the internal-age distribution of a perfectly mixed CSTR will be calculated. Equation (13-27) gives the RTD of the reactor, which upon substitution into Equation (R13.2-3) gives

Finding a relation between $E(\alpha)$ and $I(\alpha)$ 828 Chap.

$$I(\alpha) = \frac{1}{\tau} \left(1 - \int_0^\alpha \frac{1}{\tau} e^{-\alpha/\tau} d\alpha \right)$$

$$= \frac{1}{\tau} \left(1 + e^{-\alpha/\tau} \Big|_0^\alpha \right)$$

$$= \frac{1}{\tau} e^{-\alpha/\tau}$$
(R13.2-5)

True only for a perfectly mixed

Thus the internal-age distribution of a perfectly mixed CSTR is identical to the exit-age distribution, or RTD, because the composition of the effluent is identical to the composition of the material anywhere within the CSTR when it is perfectly mixed.

Example R13.2-1 CSTR with Fresh Catalyst Feed

When a catalyst is decaying, fresh catalyst must be fed to a reactor to keep a constant level of activity. The relation between catalyst weight, conversion, and catalyst activity is

$$W = \frac{F_{A0}X}{-r'_{\Delta}} = \frac{F_{A0}X}{\overline{a}k_{0}C^{n}_{\Delta}}$$
 (RE13.2-1)

where \bar{a} is the mean activity in the reactor. Determine the mean activity for first-order decay in a CSTR.

Solution

Because there will be a distribution of times the various catalyst particles have spent in the reactor, there will be a distribution of activities. The mean activity is the integral of the product of the fraction of the particles that have been in the reactor (i.e., have ages) between time α and $\alpha + \Delta \alpha$, $I(\alpha)$ $d\alpha$, and the activity at time α :

$$\bar{a} = \int_{0}^{\infty} a(\alpha)I(\alpha) d\alpha$$
 (RE13.2-2)

For first-order decay,

$$a = e^{-k\alpha} \tag{RE13.2-3}$$

In a well-mixed CSTR,

$$I(\alpha) = \frac{1}{\tau} e^{-\alpha/\tau}$$
 (R13.2-5)

$$\bar{a} = \int_0^\infty \frac{e^{-k_d \alpha} e^{-\alpha/\tau_c}}{\tau_c} d\alpha$$
 (RE13.2-4)

where k_d is the decay constant and τ_c is the mean contact time, such that

Using $I(\alpha)$ and $a(\alpha)$ to find the mean catalyst activity

$$\tau_c = \frac{W}{F_c} = \frac{\text{weight of catalyst (kg)}}{\text{feed rate of catalyst (kg/s)}}$$
(RE13.2-5)

Integrating yields

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$$\overline{a} = \frac{1}{\tau_c k_d + 1} \tag{RE13.2-6}$$

We see that for a distribution of activities, each following first-order decay in an ideal CSTR, the form of the mean activity is identical to the integrated form for second-order catalyst decay. See Problem 13-2(a). What if the catalyst decay law in Example 13-6 were second order? Third order? What if the catalyst decay law followed that of West Texas crude in Example 10–7 with $t_m=10\,$ s? What generalizations can you make?